Parametric Study of Biodiesel Production from Waste Oil

楊奇峰、吳佩學,施英隆

E-mail: 9708023@mail.dyu.edu.tw

ABSTRACT

Since the industrial revolution, the CO2 emission to the atmosphere has kept increasing year by year. The average CO2 emission per person in Taiwan is three times as much as the global average. Because biomass raw materials are produced by absorbing CO2 from the atmosphere, and the carbon cycle requires only a period from 1 to 10 years, compared to a period of millions of years for petroleum, the impact on the environment can be remarkably reduced. In this research, waste oil is used to produce biodiesel, and the results are compared against the products from the soy bean oil. It is hoped that the nature of the research fits not only the requirement of environmental protection, but also the usage of renewal energy. This thesis is aimed to explore the effects of temperature, and different catalysts (NaOH and KOH) on the production rate and the yielding quality of the biodiesel in the transesterification process using either waste oil or soy bean oil. According to experimental results, the optimal parameters for the production of biodiesel from waste oil are suggested as below. With the same catalyst, the reaction time of 120 minutes is suggested. The yield rate is 79.29% which is 17.79% higher than that for 30-minute reaction time. The MEOH/oil ratio of 6:1 is suggested. Its yield rate is85.24% and is 7.23% higher than molar ratio of 3:1. A stirring speed of 900rpm is suggested which gives a yield rate of 85.23%, and is 6.43% higher that that for 300rpm. The reaction temperature is suggested to be 60 . When the NaOH to oil ration is fixed at 0.5 wt.% and the temperature increases from 30 to 60 , the yield increases 12.11%, resulting a yield of 78.34%. By using KOH at similar conditions, it can enhance 20.84%, resulting a yield of 85.39%. In view of catalyst consumption, increasing KOH from 0.1 wt.% to 1.5 wt.% causes an increase of 37.36% in the yield, giving a yield of 85.39%. Similarly, increasing NaOH from 0.1 wt.% to 0.5 wt.% causes an increase of 25.11% in the yield, resulting a yield of 78.34%.

Keywords: Alkali Catalysis; Biodiesel; Waste Oil

Table of Contents

第一章 緒論 1.1 研究背景 1.2 研究動機 1.3 研究目的 1.4 研究架構 第二章 文獻回顧 2.1 生質柴油 2.1.1 生質柴油之優缺點 2.1.2 生質柴油的規範 2.2 生質柴油原料 2.3 轉酯化反應 2.4 鹼催化反應 2.4.1 鹼製造過程 2.5 轉酯化製程之差異點比較 2.6 轉酯化的影響因素 2.6.1 水分與游離脂肪酸的影響 2.6.2醇油比的影響 2.6.3 催化劑的影響 2.6.4 反應時間與溫度的影響 第三章 實驗材料與分析方法 3.1 實驗材料 3.2 儀器與設備 3.3 實驗方法 3.3.1油脂轉酯化參數設定 3.3.2高效液相層析(HPLC)分析 3.3.3 HPLC計算法 3.4 小型鹼催化生產參數探討 3.4.1廢油-固定催化劑反應時間之影響 3.4.2廢油-醇/油比例之影響 3.4.3廢油-轉數之影響 3.4.4廢油-氫氧化鉀催化劑用量與溫度之影響 3.4.5廢油-氫氧化鈉催化劑用量與溫度之影響 3.4.5廢油-氫氧化鈉催化劑用量與溫度之影響 3.4.6大豆油-固定催化劑反應時間之影響 3.4.7大豆油-醇/油比例之影響 3.4.8大豆油-轉數之影響 3.4.9大豆油-氫氧化鉀催化劑用量與溫度之影響 第四章 結果與討論 4.1 固定催化劑反應時間對產率的影響 4.1.1 廢油-固定催化劑反應時間對產率的影響 4.1.2 大豆油-固定催化劑反應時間對產率的影響 4.2 醇/油比例對產率的影響 4.2.1廢油-醇/油比例對產率的影響 4.2.2大豆油-轉數對產率的影響 4.3.1廢油-轉數對產率的影響 4.3.1廢油-轉數對產率的影響 4.4.4 轉酯化與氫氧化鈉用量與溫度之關係 4.4.1廢油轉酯化-氫氧化鈉與溫度之關係 4.4.4.4.5.1廢油轉酯化-氫氧化鈉與溫度之關係 4.5.2大豆油轉酯化-氫氧化鈉與溫度之關係 4.5.2兩油轉酯化-氫氧化鉀與溫度之關係 4.5.2內豆油轉酯化-氫氧化鉀與溫度之關係 第五章 結論 參考文獻

REFERENCES

[1] 教育部「技專校院發展學校重點特色暨推動技專校院整合專案」,再生能源應用之整合研發與人才培育,2005,http://www3.stut.edu.tw/project/renew/new%20energy/re_02.htm [2] 環境資訊中心,「適應基金」支助開發中國家處理全球暖化問題,2006,http://e-info.org.tw/2006/11/1122/061122A.htm [3] 王塗發,2006,因應京都議定書之產業發展-調整產業結構邁向永續經濟,http://60.248.4.115/NCSD/img/img/8795/e4-2.doc [4] 中華民國招商網經濟部投資業務處,能源,2007,

http://investintaiwan.nat.gov.tw/zh-tw/opp/inds/energy.html [5] Green County 綠色城鄉,生質柴油在車輛的應用,2007,

http://www.biodiesel-tw.org/GCB_01/GCB03.htm [6] DOE-National Energy Technology Laboratory: Home Page, 2006,

http://www.netl.doe.gov/ [7] 中央社, 因應高油價開發海底新能源, 2008, http://news.epocht imes.com.tw/8/1/11/74981.htm [8] 能源局局長葉惠青, 2004, 生質柴油示範系統兼具資源再生及潔淨能源, 經濟日報。

- [9] 台中縣環保局, 2008, 環保改善的再生燃料-生質柴油, http://bumf.teepb.gov.tw/index/i/i_013.asp?id=1115&idx=1 [10] 「生質柴油 與其它替代燃料比較與評價」,美國黃豆協會, (2003), http://www.soybean.org.tw/biodiese-10.htm.
- [11] 徐明璋,生質柴油的產製及其在柴油引擎上之可行性研究,碩士論文,國立台灣大學生物產業機電工程學研究所,2001。
- [12] 陳介武,生化柴油發展與趨勢, http://www.soybean.org.tw/tech6-3.htm, ASA/Taiwan, 2000 [13] Oak Ridge National Laboratory, ORNL
- [14] Abigor, R. D., Uadia, P. O., Foglia, T. A., Hass, M. J., Jones, K. C., Okpefa, E., Obibuzor, J. U., and Bafor, M. E., 2000. "Lipase-Catalysed Production of Biodiesel Fuel from Some Nigerian Lauric Oils", Biochem, 28: 979-981.
- [15] Pryde, E. H., 1983. Vegetable Oil as Biodiesel Fuel: Overview. J. A., Oil Chem. 60: 1557-1558.
- [16] EBB (European Biodiesel Board), 2006, http://www.ebb-eu.org/stats.php.
- [17] NBB (National Biodiesel Board), 2006, http://www.biodiesel.org.
- [18] 陳恭府, 1996, 超低硫柴油摻配生質柴油之油品特性及污染排放分析,碩士論文,高雄:國立中山大學環境工程研究所。
- [19] 吳啟明, 2001, 生質柴油燃料對直噴式柴油引擎性能及排放之研究,碩士論文,台北:國立台北科技大學車輛工程研究所。
- [20] 陳芃, 2004, 購車族的新選擇-漫談柴油車, 二月能源報導目錄:27。
- [21] DBW (Degussa Biodiesel Website), 2006, http://www.degussa4biodiesel.com.
- [22] L.C. Meher, D. Vidya Sagar, S.N.Nailk, Technical aspets of biodiesel production by transesterification-a review, 2004, sep [23] University of Idaho (Department of Biological and Agricultura Engineering). "Acute Toxicity of Biodiesel to Freshwater and Marine Organisms. Development of Rapeseed Biodiesel for Use in High-speed Diesel Engines," Progress Report, pp. 117-131, (1996).
- [24] Gerpen J.V., "Biodiesel Processing and Production." Fuel Processing Technology, VOL. 86, PP. 1097-1107, (2005).
- [25] Cole S.; Rao J.V.; Venkatacharyulu P., "Thermoacoustic Properties of Methyl Esters of N-Alkanoic Acids." Journal of American Oil Chemists' Society, VOL.72, NO. 6, PP. 687-691, (1995) [26] Infirm (AOCS), Vol.7, NO.8, 1996 [27] Peterson, C.L., 2005. In The Biodiesel Handbook; Knothe, G., Krahl, J. Gerpen, J.V., Eds.; AOCS Press: Champaign, Illinois.
- [28] 陳志威,吳文騰,「生質油之能源開發」,化工技術第147期,2005年6月。
- [29] Fukuda H; Kondo A; Noda H., "Biodiesel Fuel Production by Transesterification of Oils.", J Bioscience bioengineering, VOL.92, NO. 5, 405-416, (2001).
- [30] 吳文騰,「生物產業技術概論」,國立清華大學出版社,民92。
- [31] 吳明修,民93年六月,以廢食用油所提煉之生質柴油的油品與引擎特性研究,國立臺灣海洋大學輪機工程系碩士學位論文。
- [32] H.N.Basu and M.E.Norris, "Process for production of esters for use as a diesel fuel substitute using a non-alkaline catalyst", United States Patent:5525126,1996.
- [33] 工業技術研究院能源與資源研究所,台灣地區生質柴油應用評估, pp.12-54, 2001.
- [34] B.Freedman, E.H. Pryde and T.L.Mounts, "Variables affecting the yields of fatty esters from transesterified vegetable oil", Journal of American Oil Chemist's Society, Vol.61,pp.1638-1643,1984.
- [35] Y.Tanaka, A.Okabe and S. Ando, "Method for te preparation of a lower alkyl ester of fatty acids", United States Patent: 4303590, 1981.
- [36] L.Jeromin, E. Peukert and G. Wollmann, "Process for the pre-esterification of three acids in fats and oils", United states Patent: 4698196, 1987.
- [37] F.Ma and M.A.Hanna, "Biodiesel production:a review", bioreso- urce Technology, Vol. 70, pp.1-15,1999.
- [38] L.A.Nelson, T.A.Foglia and W.N. Marmer, "Lipase-catalyzed production of biodiesel", Journal of American Oil cheemist's Society, Vol.73(8), PP.1191-1195, 1996 [39] Y.Watanabe, Y.Shimada, A.Sugihara and Y.Tominaga, "Enzyma-Tic conversion of waste edible oil to biodiesel fuel in a fixed-bed bioreactor", Journal of American Oil Chemist's society, Vol.78(2), pp.703-707, 2001.
- [40] R.Alcantara, J.Amores, L.Canoira, E.Fidalgo, M.J.Franco and A. Navarro, "Catalytic Production of biodiesel from soybean oil, used frying oil and tallow", Biomass and Bioenergy, Vol. 18, pp. 515-527, 2000.
- [41] F.Ma, L.D.Clements and M.A. Hanna, "The effects of catalyst, free fatty acids and water on transesterification of beef tallow", American Society of Agricultural Engineers Transactions, Vol. 41(5), pp. 1261-1264, 1998.
- [42] 趙敏勳,謝明學,孫逸民,陳玉舜,劉興鑑,「儀器分析」,全威圖書有限公司,民86 [43] L.C.Meher, Vidya S.S. Dharmagadda, S.N.Nalk, Optimization of alkali-catalyzed transesterification of Pongamia pinnata oil for Production of biodiesel, 2006, Oct,