

# The Effect of Hot Dispersion on the Physical Properties of Deinked Pulp and its Application on Bleaching.

鍾武宏、彭元興

E-mail: 9607858@mail.dyu.edu.tw

## ABSTRACT

The ever increasing pulp price in the global market causes paper mills to again focus on the deinking pulp. There are, however, numerous small specks and dirt present in the deinked pulps which detract from pulp quality. Thus steam and heat dispersion are often used in later stages to reduce specks to give a more uniform optical properties. In order to understand the effects of different pulp consistencies and temperatures on the disperser performance with regard to the pulp physical and optical properties, two reducing type bleaching agents, sodium hydrosulfite and formamidine sulfinic acid (FAS) were added to the disperser stage and post-dispersion bleaching stage and their effects at different pulp consistency and temperatures on the pulp brightness and dirt speck count were examined. The study was based on 100% deinked computer form pulp. The post-dispersion physical properties examined the effect of a front stage screw press exerting different pressure to produce consistencies of 19, 32, 35 and 36%, and using steam temperatures of 90, 100, 110 and 115 °C for the treatments. The results indicate that the tensile and stiffness properties were most optimal at 100 °C; while the bursting and tear factors were most optimal at 90 °C. The attempted wax-picking test for measuring surface strength was foiled due to low values less than no. 4 wax sticks. The suggested operational temperature of 95 °C by the mill was in the right range. As for pulp consistencies, a 32% consistency was found to work well, which is akin to the 25-30% consistency suggested by the mill. The post-dispersion bleaching experiment was conducted at 40, 60, and 85 °C with different concentrations of sodium hydrosulfite and FAS. The results indicate that the optimal dosage for sodium hydro-sulfite was 0.8%. At 40 °C, the brightness gain of the resulting pulp by the sodium hydrosulfite was superior to that of FAS; at 60 °C, the gains of the 2 bleaching agents were roughly equal; whereas at 85 °C, the unbleached pulp had a brightness of 83.5% GE, while 0.8% of sodium hydrosulfite viiproduced a brightness of 88.5% GE, and 0.8% FAS dosage produced a pulp brightness of 90.5%. The results indicate that FAS performed better under higher temperatures. The on-disperser bleaching experimental results indicate that with a unbleached pulp brightness of 84% GE, a 0.1% dosage of sodium hydrosulfite produced a pulp brightness comparable to the post-disperser bleaching dosage of 0.8%, reaching 87% GE. At dosages of 0.8% sodium hydrosulfite and FAS, respectively, both boosted pulp brightness to 90% GE, a gain of 6% GE. The results of the post-disperser bleaching study indicate that the pulp dirt counts decreased with increasing bleaching agent dosages from 0.1-1.2%, regardless of the bleaching temperature. At the same dosages, the dirt counts of FAS bleached pulp tended to be fewer than the sodium hydrosulfite bleached pulp. The on-disperser bleaching study results indicate that the average dirt counts of the sodium hydrosulfite bleached pulps was 65 ppm, whereas the FAS bleached pulps had an average dirt count of 41 ppm. There was a tendency of dirt counts to increase with the increasing operational temperature of the disperser. Cost analysis of the reducing bleaching chemicals on the deinking pulp suggest that the pulp had a cost of ca. NT\$ 13000 -15000/ton. If using the optimal post-disperser bleaching temperature of 85 °C and the best brightness gain of 6% GE as a basis for calculation, then 1% dosage of sodium hydrosulfite cost NT\$ 240/ton pulp, or equal to 1.6-1.8% of the pulp cost. When FAS was used at 0.42% dosage, then the cost was NT\$ 218/ton pulp, or equal to 1.45-1.68% of the pulp cost.

Keywords : bleaching of deinked pulp; heat dispersion, sodium hydrosulfite, formamidine sulfinic acid

## Table of Contents

封面內頁 簽名頁 授權書 .....	iii	中文摘要 .....	iv	英文摘要 .....	vi
誌謝 .....	viii	目錄 .....	ix	圖目錄 .....	xiii
表目錄 .....	xvi	第一章 前言 .....	1	1.1 研究起源 .....	1
1.2 研究動機 .....	2	1.3 研究目的 .....	3	第二章 背景資料 .....	4
2.1 熱分散背景 .....	4	2.1.1 熱分散系統介紹 .....	4	2.1.2 熱分散操作參數 .....	7
2.1.3 熱分散系統後銜接 .....	7	2.1.4 各家廠商熱分散設備異同 .....	8	2.2 連二亞硫酸鈉背景 .....	10
2.2.1 反應機制 .....	11	2.2.2 生產製程 .....	13	2.2.3 應用 .....	14
2.3 甲?亞磺酸 .....	15	2.3.1 常用的生產製程 .....	16	2.4 脫墨處理及漂白藥劑 .....	16
2.4.1 氫氧化鈉 .....	17	2.4.2 矽酸鈉 .....	17	2.4.3 過氧化氫 .....	18
2.4.4 硼氫化鈉 .....	18	2.4.5 重亞硫酸鈉 .....	19	2.4.6 三聚磷酸鈉 .....	19
2.4.7 乙二胺四乙酸 .....	19				

.....20	2.4.8 二乙烯三胺五乙酸 .....	20	2.5 Kubelka-Munk 理論 .....	21	第三章 文獻回顧 .....
.....24	3.1 熱分散系統對物性的影響 .....	24	3.1.1 不同溫度與刀盤間隙對熱分散的影響 .....	24	3.1.2 在熱分散後再經由低濃度磨漿機鍊漿 應用研究 .....
.....29	3.2 還原型漂白劑甲?亞磺酸之相關文獻 .....	36	3.2.1 添加甲?亞磺酸濃度對紙張白度的影響 .....	36	3.2.2 添加甲?亞磺酸pH 值對白度的影響 .....
.....37	3.2.3 漂白時間與溫度對於白度的影響 .....	38	3.2.4 漿料濃度與漂白溫度對白度的影響 .....	38	3.2.5 漂白溫度對白度的影響 .....
.....39	3.2.6 還原型漂白劑漂白濃度對白度及回黃的影響 .....	40	第四章 實驗規劃及方法 .....	42	4.1 實驗目的 .....
.....45	4.2 實驗規劃與方法 .....	45	4.2.1 熱分散對於手抄紙物性及光學性質的影響 .....	45	4.2.2 熱分散機後及機上漂白白度及污點數應用 .....
.....51	5.1 熱分散前濃度及溫度對紙張物性及光學性質的影響 .....	51	5.1.1 游離度 .....	51	5.1.2 抗張強度 .....
.....52	5.1.3 撕力 .....	53	5.1.4 比破裂度 .....	53	5.1.5 剛挺度 .....
.....54	5.1.6 表面強度 .....	54	5.1.7 彈性模數E .....	55	5.1.8 白度 .....
.....55	5.1.9 視白度 .....	56	5.1.10 E 值 .....	56	5.1.11 不透明度 .....
.....57	5.1.12 Kubelka-Munk 理論 .....	58	5.2 熱分散機後漂白實驗 .....	60	5.2.1 機後漂白手抄紙白度安定性研究 .....
.....65	5.2.2 機後漂白污點數研究 .....	69	5.3 熱分散機上漂白實驗 .....	73	5.3.1 機上漂白還原性漂白劑手抄紙白度 安定性研究 .....
.....75	5.3.2 機上漂白污點數研究 .....	76	5.4 漂白實驗的經濟效益評估 .....	77	第六章 結論與建議 .....
.....79	6.1 物性實驗與光學實驗 .....	79	6.1.1 物性實驗 .....	79	6.1.2 光學實驗 .....
.....79	6.2 熱分散漂白實驗 .....	79	6.2.1 熱分散機後漂白實驗 .....	80	6.2.2 熱分散機後污點數研究 .....
.....80	6.2.3 熱分散機上漂白實驗 .....	80	6.2.4 熱分散機上污點數研究 .....	80	6.2.5 還原性漂白劑的成本 .....
.....81	6.3 建議 .....	81	參考文獻 .....	83	

## REFERENCES

1. 台灣區造紙工業同業公會編印, 台灣造紙工業統計2006 年年報。2. 朱志耀(1973)製漿造紙學。紙業新聞社。台北。第221-224 頁。3. 李剛、楊綠、錢超、陳新志(2006)硼氫化鈉合成新工藝研究。精細與專用化學品14(22):14-17。4. 周邦榮(2006)我國二氧化硫?企業的發展方向。精細化工原料及中間體8:13-14。5. 陳均志、唐宏科(2001)高產率甲?亞磺酸的製備。印染助劑。18(1):24-26。6. 陳慶蔚(2005)廢紙處理設備的新進展(下)。中華紙業。26(4): 38-43。7. 黃六蓮、江燕斌(2001) FAS 在機械木漿漂白中的應用。福建輕紡。16(10):24-31。8. 黃六蓮(2004)甲?亞磺酸在廢紙脫墨漿漂白中的應用。造紙化學品。16(6):66-70。9. 陸趙情、胡恒宇(2002)甲?亞磺酸楊木APMP 漂白效果的探討。中華紙業。23(11):30-32。10. 屠仁溥、沈亞勤(1995)甲酸鈉法與鋅粉法保險粉在印染應用中的效果比較。印染助劑。21(6):11-13。11. 張小平、錢宇、張獻忠(1997)保險粉在機械木漿漂白中的應用。造紙化學品。9(2): 37-36。12. 韓娜、羅洪波、張允湘、江成發(2005)濕法磷酸製取三聚磷酸鈉新工藝的研究。磷肥與複肥。20(1):16-18。13. 蘇裕昌(2000)脫墨的化學及脫墨藥劑。漿紙技術。4(4):53-65。14. Brandon C. E., Casey J. P. (1981) Strength properties of paper. Pulp and paper chemistry and chemical technology, 4 rd ed. 1819-1885. Interscience publ., New York. 15. Chester L., Szczucki C. L. and Kilgannon R. R. (1997) Peroxide reductive bleaching of mixed office waste to high brightness. Recycling. 534-539. TAPPI Press, New Orleans. 16. Christensen K., Jusheng L. (1991) Chlorine free bleaching of sulphite pulp. TAPPI Pulping Conference Proceeding. 873-879. TAPPI Press. Atlanta. 17. David L. K. (1996) Sequential bleaching of deinked paper pulp with sodium bisulfite, dithionite and borohydride US. Patent 05562803. 18. Europa Carton Hoya BRD (1991) Dispersion system trial #1, 1991/7/31. 19. Europa Carton Hoya BRD (1991) Dispersion system trial #2, 1991/8/8. 20. Fluet A. (1995) Sodium hydrosulfite brightening and colour stripping of mixed office waste furnishes. TAPPI Pulping Conference Proceeding. 717-723. TAPPI Press, Atlanta. 21. Gottsching L. and Pakarinen H. (2000) Recycled fiber and deinking. p.185. Fapet Oy. Helsinki, Finland. 22. James S. B., Anthony, G. F. (1986) Fluorescence and Kubelka-Munk theory. Appita. 39(4): 293-296. 23. Joachimides T., Hache M. (1991) Bleaching deinked pulps. Tappi J. 74(1):211 24. Jukka Heimonen. (2005) Choosing the correct DIP concept for tissue can minimize operating costs. Pulp & Paper. 79(9): 42-45. 25. Jusheng L. (1991) Bleaching of Mg-sulphite pulp with reduced effluent pollution. Ph d thesis. Norway, NTH-Trykk, ISBN 82-7119-282-5. 26. Kokta B. V., (1986) Brightening ultra-high-yield hardwood pulps With hydrogen peroxide and sodium hydrosulfite . Tappi J. (9):130. 27. Koukoulas A. A., Jordan B. D. (1997) Effect of strong absorption on the Kubelka-Munk scattering coefficient. JPPS. 23(5):224-233. 28. McCarthy C.E. (1996) TAPPI Deinking Short Course. 393-394. TAPPI Press, Atlanta. 29. Muguet M., Kogan J. (1997) Ozone bleaching of recycled paper. Recycling. 558-562. TAPPI Press, Canada 30. Reeve D. W. (1989) The principles of bleaching. Bleach plant operations seminar. 1-10. TAPPI Press, Atlanta. 31. Richard C. Denton, Gorgen A. (2002) Method of bleaching with formamidine sulfinic acid using a reducing agent to eliminate residual peroxide US Patent 6428653. 32. Ruzinsky F., Bennington C. P. (2006) Toner particle comminution in office paper dispersion. Tappi J. 5(5):7-14. 33. Rundlof M., Bristow J. A. (1997) A note concerning the interaction between light scattering and light absorption in the application of the Kubelka-Munk equations. JPPS. 23(5):220-223. 34. Singh R. P. (1979) The Bleaching of Pulp. 3rd ed. 255-273. TAPPI Press, Atlanta. 35. STFI (1984) STFI SVENSKA TRAFORSKNINGS INSTITUTET Test Report AS 63144. 1984-12-17. 36. Teodorescu G. (1992) Bleaching pressurized groundwood pulps in the grinder pit with hydrosulfite . Tappi J. (6):119. 37. Thomas H. Manley, Robert B. Johnston (1995) Screw presses in waste Dewatering. Tappi J. 78(12):112-116. 38. 亞洲地區長短纖紙漿及庫存天數走勢圖:  
[http://www.bloomberg.com/markets/asia\\_index.htm](http://www.bloomberg.com/markets/asia_index.htm) 39. 台灣區造紙同業公會:

<http://60.244.127.66/big5/tpia/o201/20030620162154-left-i.htm> 40. 鋅粉法製作保險粉，染化資訊網:

<http://www.dfmng.com.tw/member/aux-d/r01-m.htm> 41. 氫氧化鈉介紹(百度百科): <http://bk.baidu.com/view/1731.htm> 42. 重亞硫酸鈉介紹:

<http://www.htchenghua.com/1.html> 43. 乙二胺四乙酸及二乙烯三胺五乙酸介紹(造紙化學訊息網): <http://www.bigchinatech.com> 44. 保險

粉及甲?亞磺酸藥品網路報價(阿里巴巴網): <http://sdgdhg.cn.alibaba.com>